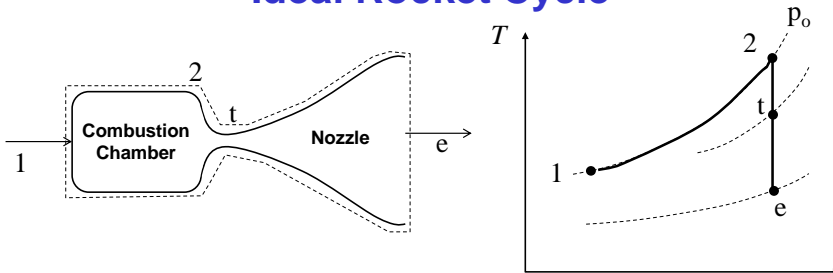


## Rocket Propulsion

### Liquid Propellant Cycles: Gas Feed and Turbopump Systems

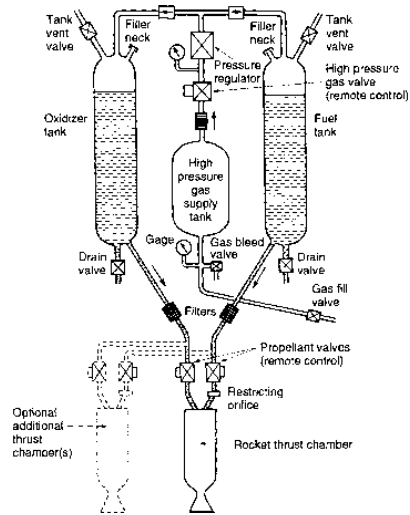
### Ideal Rocket Cycle



- How do propellants reach high pressure required by C.C. (i.e.,  $p_o$ )
  - gravity fed
    - only for low pressure applications in well-defined g field
  - pressure fed
  - turbopump fed

## Pressure Feed

- Use high pressure gas to pressurize liquid propellant tanks
- Primary controls are
  - gas pressure regulator
  - gas on/off control valve
  - liquid propellant valves

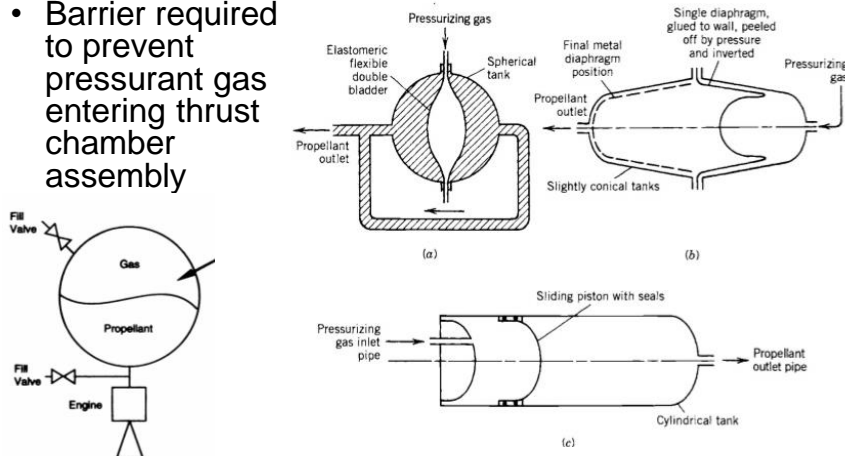


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## Positive Expulsion Tank Management

- Barrier required to prevent pressurant gas entering thrust chamber assembly



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## Turbopump Cycles

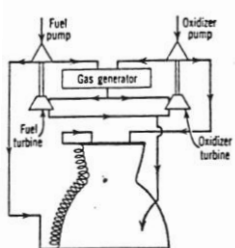
- Use pump to pressurize liquid propellants
  - steady flow pumps run with shaft power input
- Shaft power source ??
  - electric motor
    - usually insufficient onboard electrical power
  - turbine
    - need to expand high pressure, heated gas



## Liquid (Bipropellant) Cycles

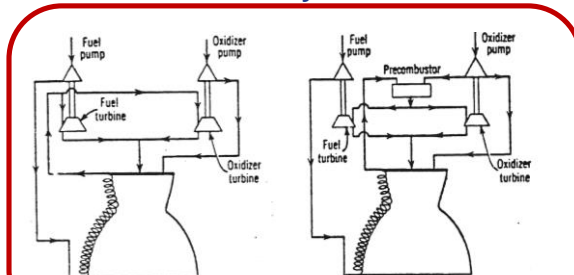
- Various rocket cycles have been developed that differ on how hot gas is supplied to the turbines
- Most common are variations of:

### Open Cycle



Gas Generator Cycle

### Closed Cycles

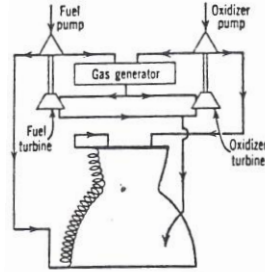


Expander Cycle

Staged Combustion Cycle

## LRE Pump-Fed Open Cycles

- Turbine exhaust gas can't be re-injected into comb. chamber (pressure too low)  $\Rightarrow$  lower  $I_{sp}$ 
  - turbine exhaust dumped through separate nozzle or injected in downstream part of main nozzle (where pressure is low)
- Generally rely on low flow rate, few % of total propellant flow (less wasted propellant mass) and high pressure drop across turbine

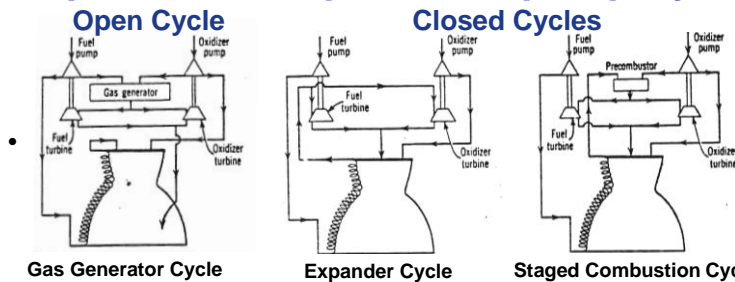


Gas Generator Cycle

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## Comparison of Liquid Turbopump Cycles



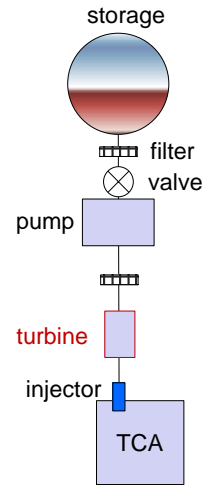
	Open Cycle	Closed Cycles	
	<b>Gas Generator Cycle</b>	<b>Expander Cycle</b>	<b>Staged Combustion Cycle</b>
<b>Isp</b>	low	medium	high
<b>Complex</b>	medium	low	high
<b>Thrust</b>	high	Low	high
<b>P<sub>r</sub> Turbine</b>	high	Medium	low
<b>Examples</b>	V2, F-1/J-2 (SaturnV), Vulcain (Ariane 5), RS-68 (Delta IV), Merlin 1 (Falcon)	Upper Stages: RL-10 (Saturn IV, Delta III, IV), Vinci (Ariane 6)	RS-25 (SSME), NK-33 (N-1, Soyuz), RD-170 (Energia), RD-180 (Atlas V), BE-4 (Atlas V?), AR1 (Atlas V?), Raptor (ITS?)

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## Pressure Losses in Propellant Path

1. Storage pressure
2. Dynamic pressure loss
  - static pressure drops as flow moves
3. Line losses between storage and pump
  - friction losses in piping
  - pressure drops in flow restrictions (orifices, filters, valves, etc.)
4. Pump increase
5. Line losses
6. Turbine pressure drop
7. Injector pressure drop

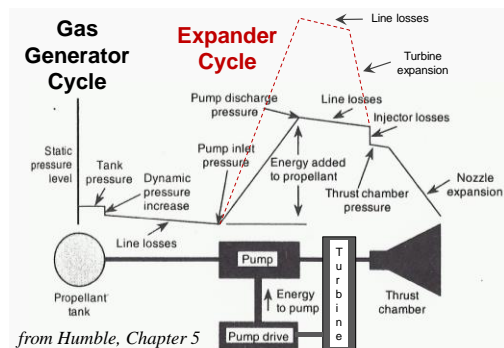


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## Pressure Requirements

- Significant difference between cycles is the pump pressure requirement
  - for example, an open vs. a closed cycle
  - higher pump pressure required if propellant stream passes through turbine before entering combustion chamber



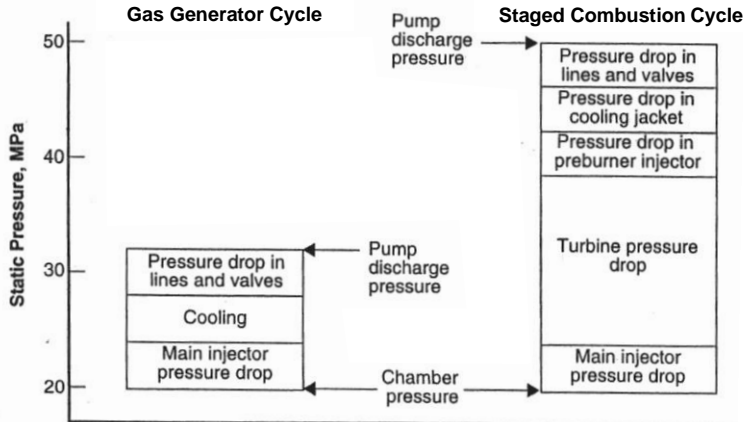
from Humble, Chapter 5

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## Example Pump Pressure Requirements

- Pump must produce an additional 180 bar for the closed cycle in this comparison with a c.c. pressure of 200 bar



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## Pressure Modeling – “Rules of Thumb”

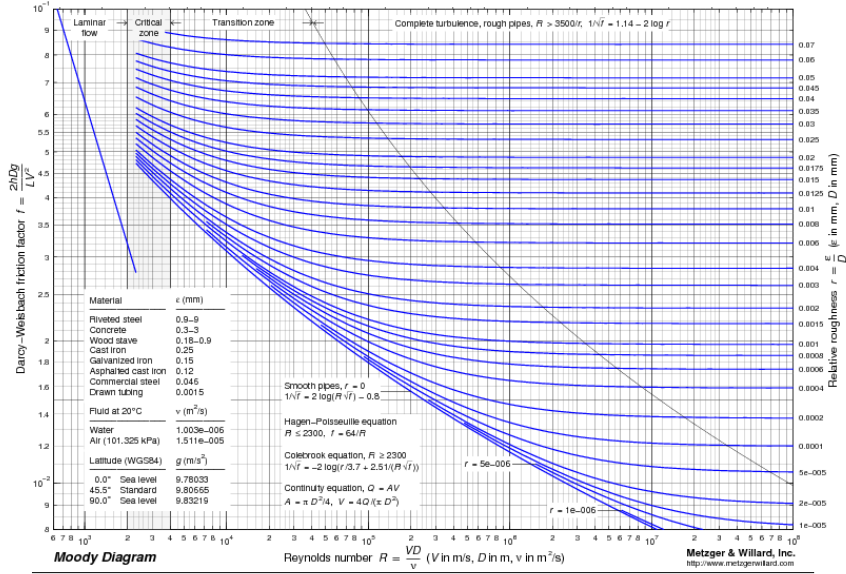
- **Dynamic pressure**  $\Delta p = \frac{1}{2} \rho u^2$  (IV.20)
- **Line losses: piping**
  - various modeling approaches, e.g., friction factor
  - traditional expression
 
$$\Delta p_f = \rho g_o H_f \quad H_f = f \frac{L}{d} \frac{u^2}{2g_o}$$

Head Loss (height)  $\rightarrow$  (Darcy)  $\rightarrow$  friction factor  $\rightarrow$  pipe length  $\rightarrow$  pipe diameter
  - or  $\Delta p_f = f \rho (L/d) (u^2/2)$  (IV.21)
  - $f$  is function of  $Re_d$ , pipe material, surface finish
    - find values from Moody diagrams, empirical models

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# Moody Diagram



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## Pressure Modeling – “Rules of Thumb”

- **Line losses: orifices**
  - flow restrictors, valves, etc.
  - typically use discharge coefficient

$$(IV.22a) \quad C_d = \frac{Q}{A\sqrt{2\Delta p/\rho}} = \frac{\dot{m}/\rho}{A\sqrt{2\Delta p/\rho}}$$

volumetric flowrate

orifice area

alternate definition  
 $C_d = \frac{Q}{A\sqrt{\Delta p/\rho}}$

- essentially ratio of actual flow rate to flow rate through ideal “nozzle” that produces same expansion
  - so pressure drop given by  $\Delta p = \frac{(\dot{m}/AC_d)^2}{2\rho}$
- $$(IV.22b) \quad \Delta p = \frac{(\dot{m}/AC_d)^2}{2\rho} \quad \Delta p = \frac{(\dot{m}/AC_d)^2}{\rho}$$

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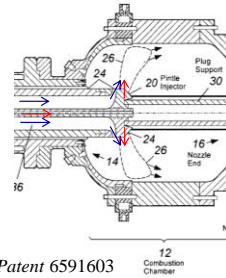
## Pressure Modeling – “Rules of Thumb”

- **Typical line losses**

- feed system:  $\Delta p_{loss} = 10$ 's kPa (4-8 psi)
- regenerative cooling (of TCA):  $\Delta p_{loss} \sim 10-20\%$  of  $p_{cc}$

- **Injector pressure drops**

- required to produce required dispersion and mixing of propellant, isolation, etc.
- depends on engine operational requirements and propellant type
  - $\Delta p_{loss} \sim 20\%$   $p_{cc}$  for unthrottled engines
  - $\Delta p_{loss} \sim 30\%$   $p_{cc}$  for throttled engines
  - as low as  $\Delta p_{loss} \sim 5\%$   $p_{cc}$  for some pintle injectors



US Patent 6591603

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## Pressure Modeling – “Rules of Thumb”

- **Turbine pressure drops**

- amount based on the required pressure ratio across turbine to supply pump power
 
$$Pr_t = \frac{P_{t,inlet}}{P_{t,exit}}$$
- gas generator cycle:  $Pr_t$  up to  $\sim 20$ 
  - low flow rate so large expansion requirement
- staged, expander cycles: lower  $Pr_t \sim 1.3-1.7$ 
  - often includes complete flow from one of the propellant streams

- **Pump requirements**

(IV.23)

- pump supply pressure
- pump inlet pressure

$$P_{pump,exit} = p_{cc} + \Delta p_{inj} + \Delta p_{lines}$$

$$P_{pump,inlet} = p_{storage} - \Delta p_{dyn} - \Delta p_{lines}$$

$$\Delta p_{pump} = P_{pump,exit} - P_{pump,inlet}$$

pump power requirement



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## Pump Power Requirements

- Conservation equations**

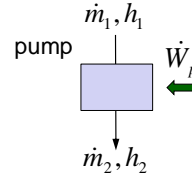
- assume steady flow, adiabatic

- mass:  $\dot{m}_1 = \dot{m}_2 \equiv \dot{m}$

- energy  $\dot{m}h_1 + \dot{W}_p = \dot{m}h_2$  ?

$$\dot{W}_p = \dot{m}(h_2 - h_1) = \dot{m}c_p(T_2 - T_1)$$

*NO, not perfect gas*



- State equations**

$$h \equiv e + p/\rho \quad dh = de + d(p/\rho)$$

$$dh = cdT + \frac{dp}{\rho} \quad \text{assume incompressible liquid } \rho \neq \rho(p)$$

Gibbs' Eqn.

$$Tds = dh - \frac{dp}{\rho} \quad \text{if isentropic} \Rightarrow dh = \frac{dp}{\rho} \quad dT = 0$$

## Pump Power Requirements

- Ideal pump power**

- so for incompressible liquid undergoing ideal (adiabatic, isentropic) pumping

$$\dot{W}_{p,ideal} = \dot{m}\Delta h_{ideal} = \dot{m} \frac{\Delta p_{pump}}{\rho_l}$$

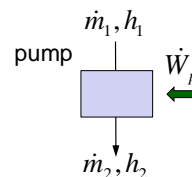
- Pump efficiency** *for same Δp across both*

$$\eta_p \equiv \frac{\dot{W}_{p,ideal}}{\dot{W}_{p,actual}} = \frac{\Delta h_{ideal}}{\Delta h_{actual}} \quad \text{typical } \sim 70\text{-}90\%$$

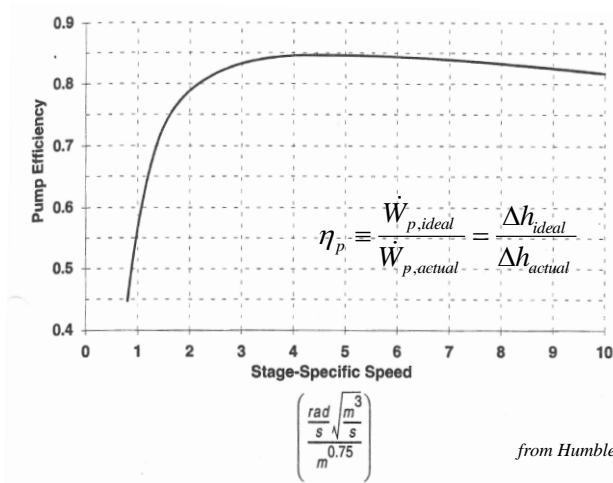
- Pump power**

*in terms of pump head*

$$(IV.24) \quad \dot{W}_p = \frac{\dot{m}\Delta p_{pump}}{\eta_p \rho} = \frac{\dot{m}g_o H_{pump}}{\eta_p}$$



## Example Pump Characteristics



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## Turbine Power Requirements

- Power output needed**

- depending on shaft/gear box efficiency

$$\dot{W}_t \geq \dot{W}_p$$

- Conservation equations (steady, adiabatic)**

- mass:  $\dot{m}_1 = \dot{m}_2 \equiv \dot{m}$

- energy  $\dot{m}h_{o1} = \dot{m}h_{o2} + \dot{W}_t \Rightarrow \dot{W}_t = \dot{m}(h_{o1} - h_{o2})$

- for cal. perfect gas  $\dot{W}_t = \dot{m}c_p(T_{o1} - T_{o2})$

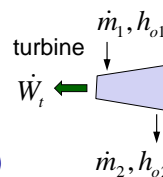
- Turbine efficiency**

- if also reversible (so isen.)  $Pr_t = p_{o1}/p_{o2} = (T_{o1}/T_{o2s})^{\gamma/(\gamma-1)}$

$$\eta_t \equiv \frac{\Delta h_{actual}}{\Delta h_{ideall}} \Rightarrow \dot{W}_t = \dot{m}c_p T_{o1} \eta_t (1 - Pr_t^{(1-\gamma)/\gamma}) \quad \text{(IV.25)}$$

for same pressure ratio

$$\dot{W}_{t,ideal} = \dot{m}c_p(T_{o1} - T_{o2s})$$

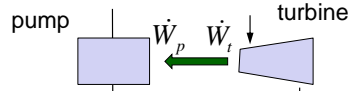


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## Power Summary

- **Power requirements**



$$\dot{W}_p = \frac{\dot{m}_l \Delta p_{pump}}{\eta_p \rho_l} = \eta_{trans} \dot{W}_t = \eta_{trans} \dot{m}_t c_p T_{o,t,inlet} \eta_t (1 - Pr_t^{(1-\gamma)/\gamma})$$

shaft or gear transmission efficiency

– so given

- pump flow rate
- pump pressure rise
- pump and turbine efficiencies

– have relation between

- turbine inlet temperature
- turbine pressure ratio
- turbine flow rate

*can be linked*