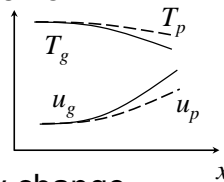


Solid Rocket Motors

Two-Phase Flow in Nozzles

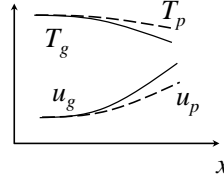
Two Phase Flow in Nozzles

- Common for SRM to have droplets or solid particles (e.g., Al_2O_3 and soot) from propellant flowing through nozzle
 - how does 2-phase flow change T (energy), velocity (momentum) of nozzle flow
- Nozzle = expansion
- What can happen?
 - in accelerating flow, particle has inertia – lags flow velocity change
 - in cooling flow, particle not expanding – temperature drop lags due to thermal inertia



Two Phase Flow in Nozzles

- How do particles “catch up” to gas changes?
- Velocity - drag
 - $u_p \uparrow, u_g \downarrow$
- Temperature – heat transfer
 - $T_p \downarrow, T_g \uparrow (\Rightarrow u_g \uparrow)$
- Thrust effect



$$\tau \sim \dot{m}u_e = \dot{m}_g u_{e,g} + \dot{m}_p u_{e,p}$$

- velocity
 - overall velocity lower due to particles
- mass flow rate
 - overall mass flow rate increased by particles

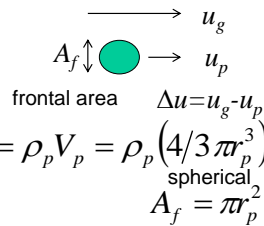
Velocity Lag - Model Approach

- Drag

$$F_D = C_D A_f \frac{1}{2} \rho_g (\Delta u)^2$$

$$= m_p \frac{du_p}{dt}$$

$$\frac{du_p}{dt} = \frac{3}{8} C_D \frac{\rho_g}{\rho_p} \frac{(\Delta u)^2}{r_p}$$



- $C_D = ?$
 - small particles \Rightarrow laminar or Stokes flow
 - Stokes $C_D \sim 24/Re$
 - laminar $C_D \sim \frac{24}{Re} (1 + a Re^b)$

Drag Model

- For Stokes flow, need $Re < \sim 2$

$$\frac{du_p}{dt} = \frac{9}{2} \frac{\mu_g}{\rho_p} \frac{\Delta u}{r_p^2}$$

$$\Delta u \sim 10 \text{ m/s}$$

$$\rho_g \sim 1-10 \text{ kg/m}^3$$

$$\mu_g \sim 5 \times 10^{-5} \text{ kg/m/s}$$

$$\Rightarrow d_p < 2-20 \mu\text{m}$$

- not dependent on gas density
- acceleration
 - $\propto 1 / \text{particle area}$
 - $\propto \text{velocity difference}$
- For laminar flow
 - weak function of ρ_g , $1/\text{area}^n$ ($n < 2$), $\Delta u^{1.5}$

Particle Velocity Lag in a Nozzle

- For high temperature rocket nozzle flows
 - typical

$$du_g/dt \sim O(10^7 \text{ m/s}^2)$$

$$\frac{du_p}{dt} = \frac{9}{2} \frac{\mu_g}{\rho_p} \frac{\Delta u}{r_p^2}$$

- Assuming Stokes flow and
 - $\rho_p \sim O(10^3 \text{ kg/m}^3)$, $\mu_g \sim O(10^{-4} \text{ kg/m/s})$
 - need $r_p < O(0.1 \mu\text{m})$ for no velocity lag
 - so no lag for “smoke” particles
 - large particles (e.g., agglomerates) can have significant velocity lag

Temperature Lag - Model Approach

- Heat transfer (negl. radiation)

$$\dot{Q} = hA_s(T_p - T_g)$$

$$= -m_p c \frac{dT_p}{dt}$$

$\Delta u \rightarrow$

$A_s = 4\pi r_p^2$

$m_p = 4/3 \pi r_p^3 \rho_p$

spheres

laminar flow

$$h \sim \frac{k_g}{d_p} \left(2 + a \text{Re}^{0.5-0.6} \text{Pr}^{0.3-0.4} \right)$$

low Re

$$h \sim k_g / r_p$$

$$\frac{dT_p}{dt} = \frac{-3k_g}{c\rho_p} \frac{\Delta T}{r_p^2}$$

– particle temperature lag scales with r_p^2

Particle Temperature Lag in a Nozzle

- For high temperature rocket nozzles

– typical $dT_g/dt \sim O(1000 \text{ K} / 1 \text{ ms})$

$$\frac{dT_p}{dt} = \frac{-3k_g}{c\rho_p} \frac{\Delta T}{r_p^2}$$

- Assuming low Re flow and

$$k_g \sim O(10^{-1} \text{ W/mK}), \rho_p \sim O(10^3 \text{ kg/m}^3), c \sim O(1 \text{ kJ/kgK})$$

$$\Rightarrow 3k_g / c\rho_p \sim (1-5) \times 10^{-7} \text{ m}^2/\text{s}$$

– for small temperature lag

- for $r_p \sim 5 \mu\text{m}$, $\Delta T \sim$ few hundred K

- for $r_p \sim 0.3 \mu\text{m}$, $\Delta T \sim 1 \text{ K}$

– *smoke at same temperature as gas*

Specific Impulse

- Can solve flow through nozzle using separate energy and momentum equations for gas and particles
 - include drag and heat transfer exchanges
- Limiting case example (particle size independent)
 - gas: $T_o=2780$ K, $\gamma=1.2$, $MW=25$
 - particle loading: 10% (by mass), $c\sim 2$ kJ/kgK
 - nozzle: $p_o=50$ atm, $p_e=1$ atm

	No particles	No u lag		∞ u lag	
		No T lag	∞ T lag	No T lag	∞ T lag
Isp (s)	236	228	224	216	213

results from Hill and Peterson

Particles can't expand

No lags – still have "loss" (3%)

T lag smaller effect

vel. lag has significant effect (9% "loss")