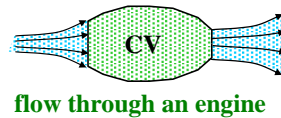
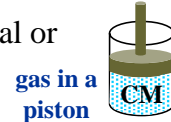




Thermodynamic Systems

- **Systems**
 - a **finite portion of matter** *or* **restricted portion of space** that we wish to examine
- **Control Mass** (Lagrangian Approach)
 - fixed portion of *matter* surrounded by real or imaginary boundaries
 - *matter can not cross boundary*
- **Control Volume** (Eulerian Approach)
 - volume of *space* surrounded by real or imaginary boundaries
 - *matter can cross boundary*



Conservation Equations

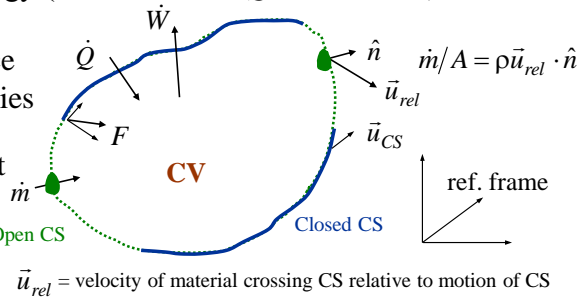
- Govern mechanics and thermodynamics of systems
- Control Mass Laws
 - **mass**: can not create or destroy mass (e.g., neglect nuclear reactions)
 - **momentum**: Newton's Law, $F=ma$
 - **energy**: 1st Law of thermodynamics, $dE=\delta Q-\delta W$
 - **entropy**: 2nd Law, $dS=\delta Q/T+\delta P_s$
- Propulsion systems generally employ fluid flow
 - need to write conservation laws in terms for **Control Volumes**



Reynolds Transport Theorem - RTT

- Provides general form for converting **conservation laws** from control mass to **control volumes**
- Take arbitrary control volume (**CV**); can be moving
 - mass and energy (“heat” transfer Q and work W) can cross **control surface (CS) boundaries**

- forces also act on CS and mass in CV



RTT Equation

- Take any **extensive property B**, that follows a “conservation” law and its **intensive version β** (per mass); can show

$$\left. \frac{dB}{dt} \right|_{CM} = \frac{d}{dt} \int_{CV} \rho \beta dV + \int_{CS} \rho \beta (\vec{u}_{rel} \cdot \hat{n}) dA \quad (II.1)$$

Replace with appropriate Conservation Law Storage term (rate of increase inside CV) Net flux of property leaving CV, carried by flow (outflow - inflow)

- Always leads to **PICO** relationship

$$\text{Production} + \text{Input} = \text{Change (in time)} + \text{Output}$$



Mass Conservation

- If property of interest is mass

$$B = m, \quad \beta = \frac{dB}{dm} = \frac{d(m)}{dm} = 1$$

- From **RTT**

$$\left. \frac{dB}{dt} \right|_{CM} = \frac{d}{dt} \int_{CV} \rho \beta dV + \int_{CS} \rho \beta (\vec{u}_{rel} \cdot \hat{n}) dA$$

$$\left. \frac{d(m)}{dt} \right|_{CM} = \frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho (\vec{u}_{rel} \cdot \hat{n}) dA$$

- CM:** $\left. \frac{d(m)}{dt} \right|_{CM} = 0$

Integral Control Volume Form of Mass Conservation

- CV:**

$$0 = \frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho (\vec{u}_{rel} \cdot \hat{n}) dA \quad (\text{II.2})$$



Simplified Mass Conservation

$$0 = \frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho (\vec{u}_{rel} \cdot \hat{n}) dA$$

- Uniform flow (at CS)** - no variations across flow

$$\int_{CS(t)} \rho (\vec{u}_{rel} \cdot \hat{n}) dA = \sum_{outlets} \rho u_{rel} A - \sum_{inlets} \rho u_{rel} A$$

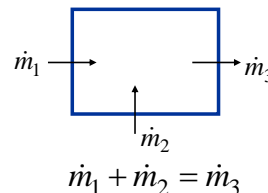
$$= \sum_{outlets} \dot{m} - \sum_{inlets} \dot{m}$$

- Add **Steady-State**

$$\frac{d}{dt} \int_{CV} \rho dV = 0$$

$$\Rightarrow \sum_{outlets} \dot{m} = \sum_{inlets} \dot{m}$$

~~PI=CO~~ → **Input = Output**





Conservation of Momentum

- Linear momentum

$$\vec{B} = m\vec{u}, \quad \vec{\beta} = \vec{u}$$

- RTT then gives

$$\left. \frac{d(m\vec{u})}{dt} \right|_{CM} = \frac{d}{dt} \int_{CV} \rho \vec{u} dV + \int_{CS} \rho \vec{u} (\vec{u}_{rel} \cdot \hat{n}) dA$$

- Use Newton's Law

$$\left. \frac{d(m\vec{u})}{dt} \right|_{CM} = \sum \vec{F}$$

total force acting on fluid

$$\sum \vec{F}_{CV} = \frac{d}{dt} \int_{CV} \rho \vec{u} dV + \int_{CS} \rho \vec{u} (\vec{u}_{rel} \cdot \hat{n}) dA$$

momentum transferred to fluid

Input = Change + Out - In $\cancel{PI=CO}$

Conservation Equations - 7

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AE4451 Propulsion



Force Terms

- Examine different forces that can act on matter in our control volume

$$\sum \vec{F}_{onCV} = \sum \vec{F}_{body\ onCV} + \sum \vec{F}_{surface\ onCS}$$

e.g., gravity

e.g., pressure, shear, ...

- Body forces

$$\vec{F}_{body} = \int_{CV} \rho \vec{f} dV \quad \text{with } \vec{f} = \text{body force/mass, i.e., acceleration}$$

- Surface forces

- free surfaces: not connected to solid body crossing control surface
- connected surfaces: solid boundaries where there are reaction forces

Conservation Equations - 8

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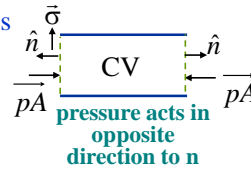


Surface Forces

- Free surfaces

$$\vec{F}_{surface} = \oint_{CS} p \hat{n} dA + \int_{CS} \vec{\sigma}_{shear} dA$$

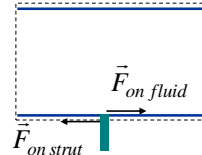
normal stress shear stress
0 if inviscid



- Connected solid surfaces

– force on fluid is reaction force (inverse) of force on solid body

$$\vec{F}_{on\ fluid} = -\vec{F}_{on\ solid\ body}$$



- Combine Integral Control Volume Form of Momentum Conservation

$$\vec{F}_{solid\ body\ on\ fluid} - \int_{CS} p \hat{n} dA + \int_{CS} \vec{\sigma}_{shear} dA + \int_{CV} \rho \vec{f} dV = \frac{d}{dt} \int_{CV} \rho \vec{u} dV + \int_{CS} \rho \vec{u} (\vec{u}_{rel} \cdot \hat{n}) dA \quad (II.3)$$



Conservation of Energy

- Energy: microscopic + macroscopic forms of energy

$$B = E_o = E + E_{kinetic} = E + \frac{1}{2} mu^2$$

energy per mass → $\beta = e_o = e + \frac{u^2}{2}$

- RTT then gives

$$\left. \frac{d(E_{tot})}{dt} \right|_{CM} = \frac{d}{dt} \int_{CV} \rho e_{tot} dV + \int_{CS} \rho e_{tot} (\vec{u}_{rel} \cdot \hat{n}) dA$$

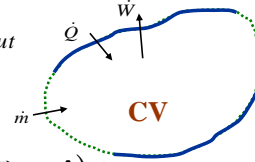
- Use 1st Law Thermodynamics for energy conservation of control mass



1st Law of Thermodynamics

- Differential form $dE_{CM} = \delta Q_{in} - \delta W_{out}$

$$\left. \frac{dE}{dt} \right|_{CM} = \frac{\delta Q_{in}}{dt} - \frac{\delta W_{out}}{dt} = \dot{Q}_{in} - \dot{W}_{out}$$



- Into RTT

$$\dot{Q}_{in} - \dot{W}_{out} = \frac{d}{dt} \int_{CV} \rho e_o dV + \int_{CS} \rho e_o (\vec{u}_{rel} \cdot \hat{n}) dA$$

- But work is related to forces ($F \cdot x$) acting on CV
 - already examined some kinds of forces
 - let’s relate them to work terms



Work and Forces

- Relationship

$$\dot{W} = \vec{F} \cdot \frac{d\vec{x}}{dt} = \vec{F} \cdot \vec{u}$$

Since we defined work as positive when done **BY** fluid

- Body forces**

$$\dot{W}_{body} = \int_{CV} \rho \vec{f} \cdot \vec{u} dV$$

- Fluid forces** (stresses)

“Flow Work”

$$\dot{W}_{press} = \int_{CS} p(\vec{u} \cdot \hat{n}) dA$$

$$\dot{W}_{shear} = - \int_{CS} \vec{\sigma} \cdot \vec{u} dA$$

- Reaction Forces**

– lump into “useful” work term, e.g., shaft work

$$\dot{W}_{shaft}$$



Energy Conservation

- Combine into RTT result (*neglect shear forces*)

$$\dot{Q}_{in} - \dot{W}_{shaft} + \int_{CV} \rho \vec{f} \cdot \vec{u} dV - \int_{CS} p(\vec{u} \cdot \hat{n}) dA = \frac{d}{dt} \int_{CV} \rho e_o dV + \int_{CS} \rho e_o (\vec{u}_{rel} \cdot \hat{n}) dA$$

Combine flow work and energy flux
Similar Form
Stagnation Enthalpy

$$\rho e_o + \rho \frac{p}{\rho} = \rho \left(e_o + \frac{p}{\rho} \right) = \rho h_o \quad h_o = h + \frac{u^2}{2}$$

$$\dot{Q}_{in} - \dot{W}_{shaft} + \int_{CV} \rho \vec{f} \cdot \vec{u} dV - \int_{CS} p(\vec{u} - \vec{u}_{rel}) \cdot \hat{n} dA = \frac{d}{dt} \int_{CV} \rho e_o dV + \int_{CS} \rho h_o (\vec{u}_{rel} \cdot \hat{n}) dA$$

- For reference frame moving with control volume at *constant velocity and no body forces*

$$\dot{Q}_{in} - \dot{W}_{shaft} = \frac{d}{dt} \int_{CV} \rho e_o dV + \int_{CS} \rho h_o (\vec{u} \cdot \hat{n}) dA \quad (II.4)$$

In - Out
Change
Out - In, of energy in mass